

MULTI-SCALE UNCERTAINTY ANALYSIS

A tool to systematically consider variability in
lignocellulosic bioethanol processes



Bioethanol in a circular economy



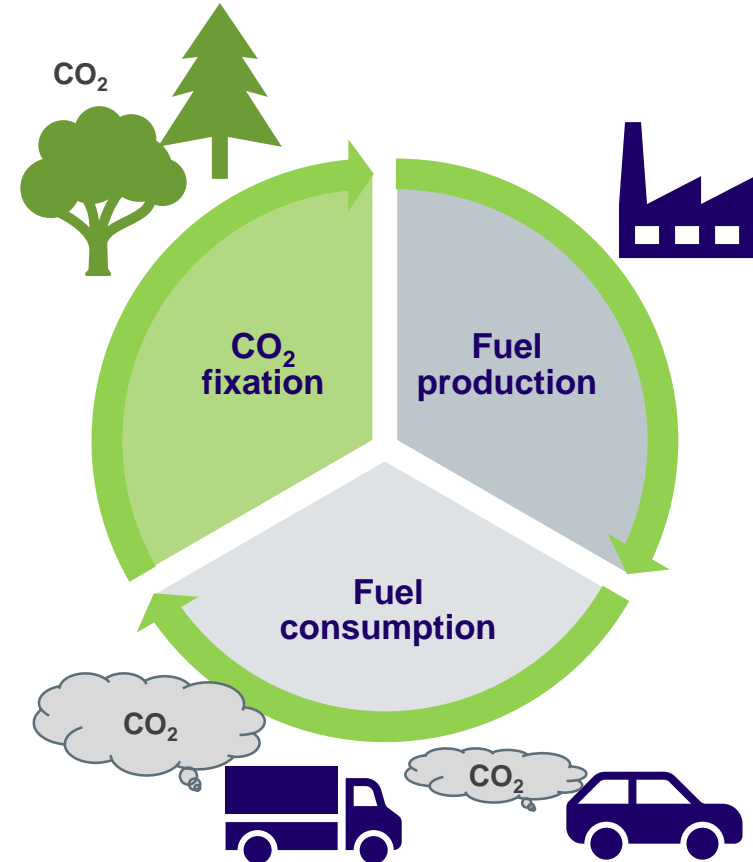
Usage of **fossil fuels** steadily increasing



ca. 50% is used for transportation



Bioethanol sustainable alternative to fossil fuels



Variability in the bioethanol process

Raw materials



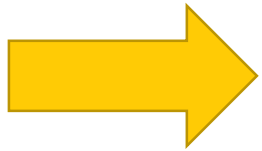
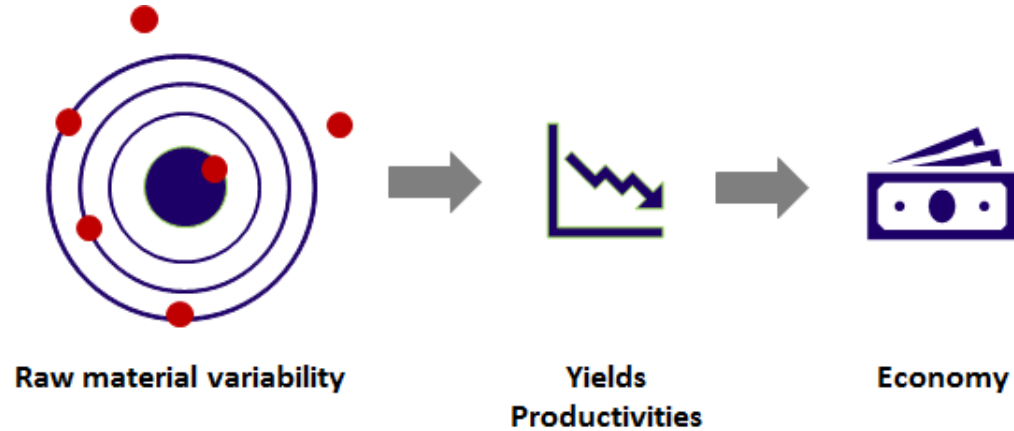
- 🎯 **Location**
- 🎯 **Harvest time**
- 🎯 **Composition of biomass**
- 🎯 **Storage**

Measurement and control



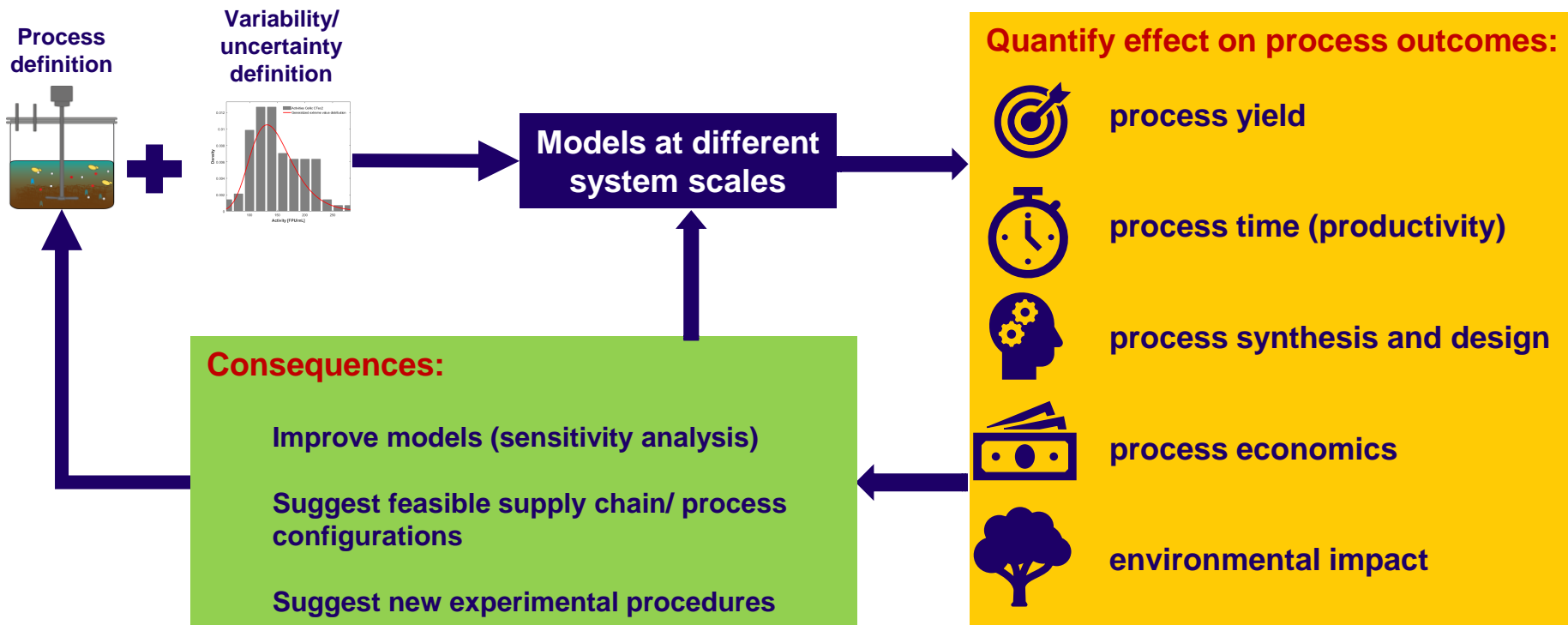
- 🎯 **High turbidity**
- 🎯 **Local viscosity differences**
- 🎯 **Solid compounds in liquid mixture**
- 🎯 **Complex chemical reaction system**

Effect of variability on process

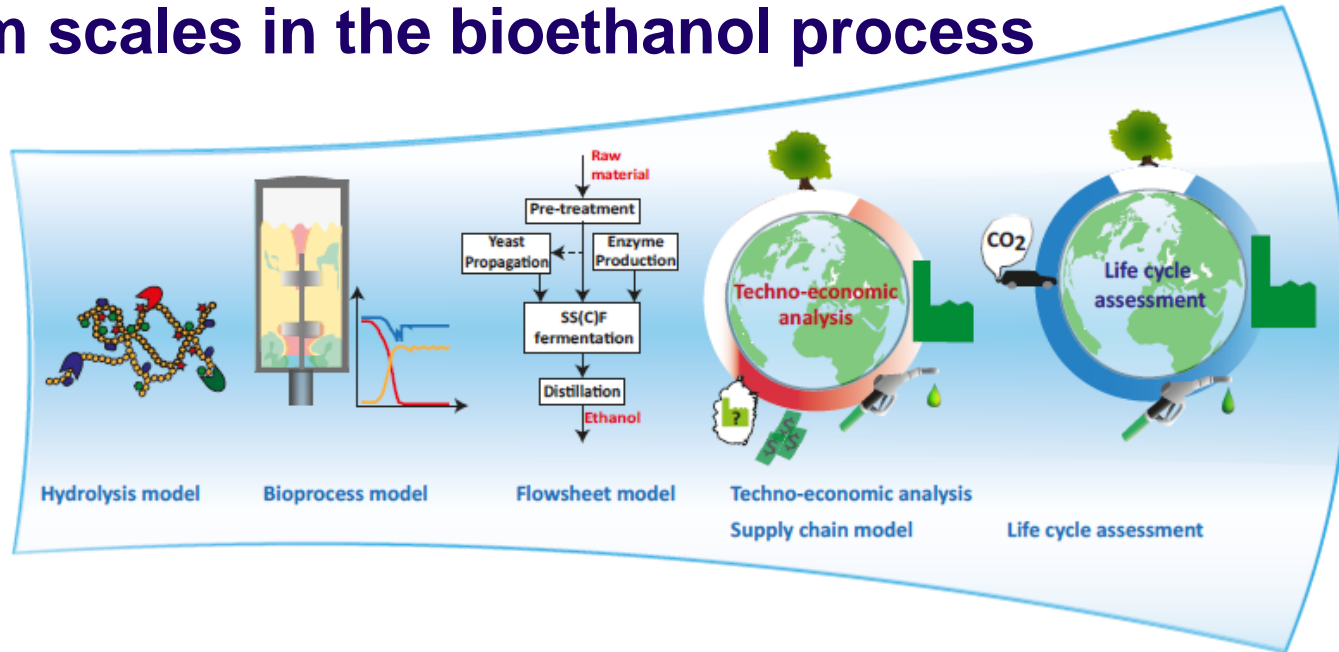


Integrate variability in process development at different scales!

Multi-scale uncertainty analysis – results & objectives

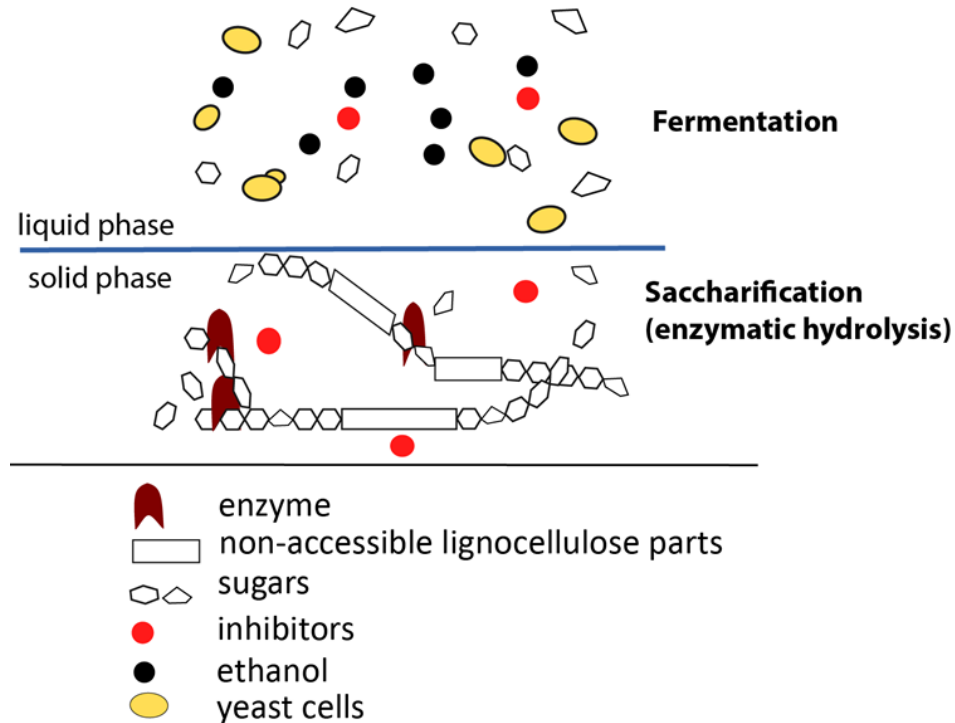


System scales in the bioethanol process



Macro-molecular scale	Bioprocess scale	Factory scale	Global scale	Global scale
describe enzyme action	describe bioprocess	describe process integration	describe cost and profits	describe environmental impact
maximize hydrolysis yield develop enzyme cocktail	develop bioprocess perform optimal experimental designs perform optimal control	develop process synthesis and design	develop supply chain select economically best process alternative(s)	develop process based on environmental impact

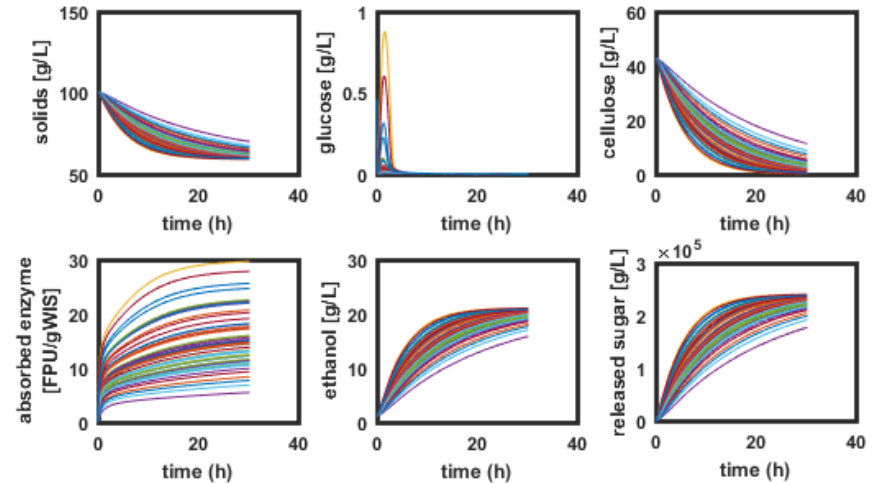
The bioprocess



The bioprocess/ hydrolysis model

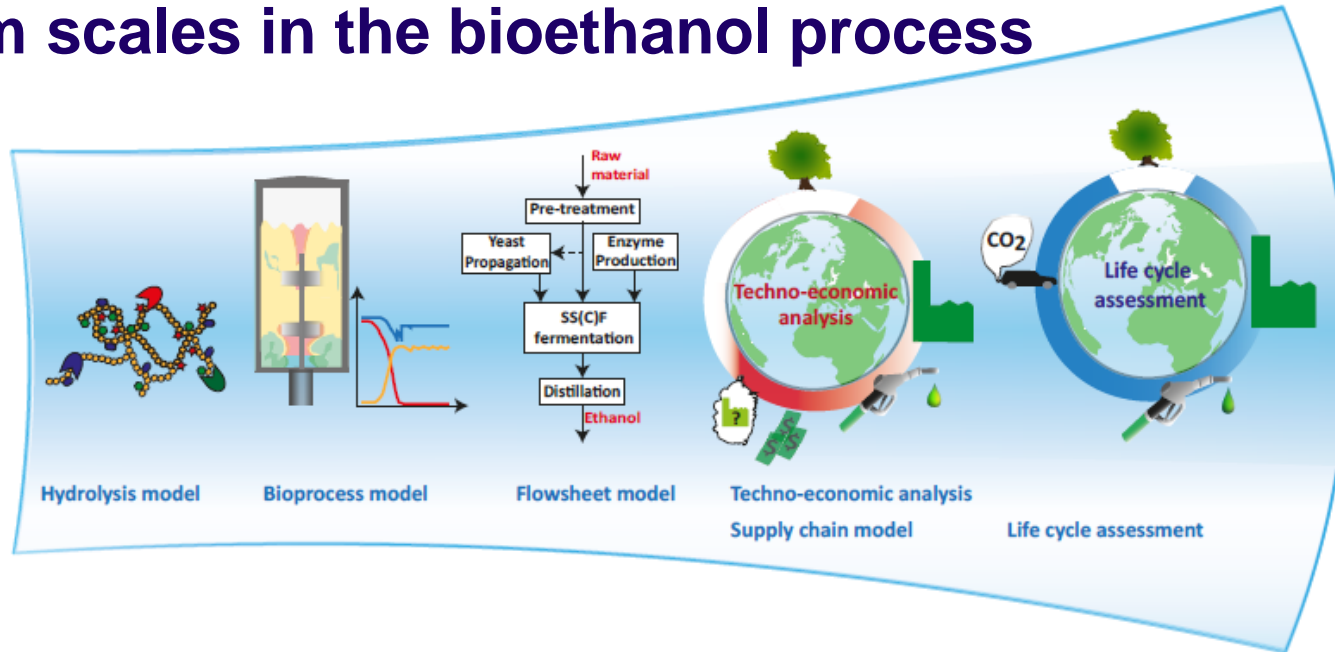
- ❑ Macro-kinetic model consisting of
 - 8 differential equations
 - 4 explicit algebraic equations

- ❑ Numerical solution in MATLAB using ode15s solver for stiff problems



Simulation results for selected state variables for a batch process at demo plant (10m³) scale

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Flowsheet model and techno-economic analysis

Bioprocess model

OLE server

Process yields

VBA

SuperPro Designer

FERMENT-1 (Continuous Stoich. Fermentation) in P-33

Oper. Cond's | Volumes | Reactions | Vent/Emissions | Labor, etc. | Description

Reaction Data

Name: Hydrolysis cellulose Parallel? ☐

Reaction Limiting Comp.: Cellulose

Conversion Achieved: 74.00 %

Reaction Progress

☐ Set Conversion: 93.00 %

Based on: ☐ Reaction Limiting Component

☐ Ref. Comp.: Cellulose

Conversion Achieved: 74.00 %

☐ Calculate to Achieve Target Concentration

0.0000 kg/m³ of (none)

Reaction Heat Ignore ☒

Assume zero reaction heat at the enthalpy calculation reference temperature (0.0 °C).

Fermentation Mass Stoichiometry

162.16 Cellulose + 18.02 Water → 180.15 Glucose

Stoichiometry Balance for Hydrolysis cellulose

Reactants

	Component	Mass Coeff.
1	Cellulose	162,1600
2	Water	18,0150

Total Mass: 180,175

Products

	Component	Mass Coeff.
1	Glucose	180,1570

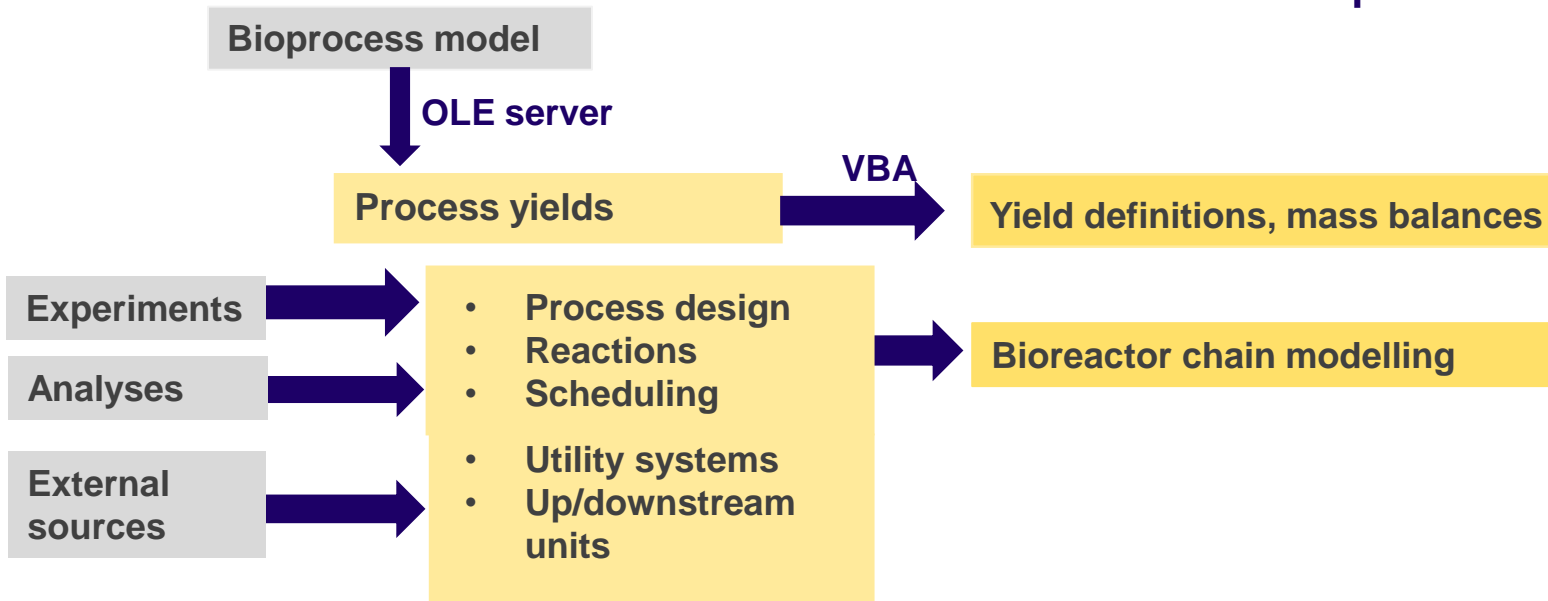
Total Mass: 180,157

Stoichiometric Coefficients: ☐ Mass ☐ Molar

OK Cancel Help

Flowsheet model and techno-economic analysis

SuperPro Designer



Flowsheet model and techno-economic analysis

Bioprocess model

OLE server

Process yields

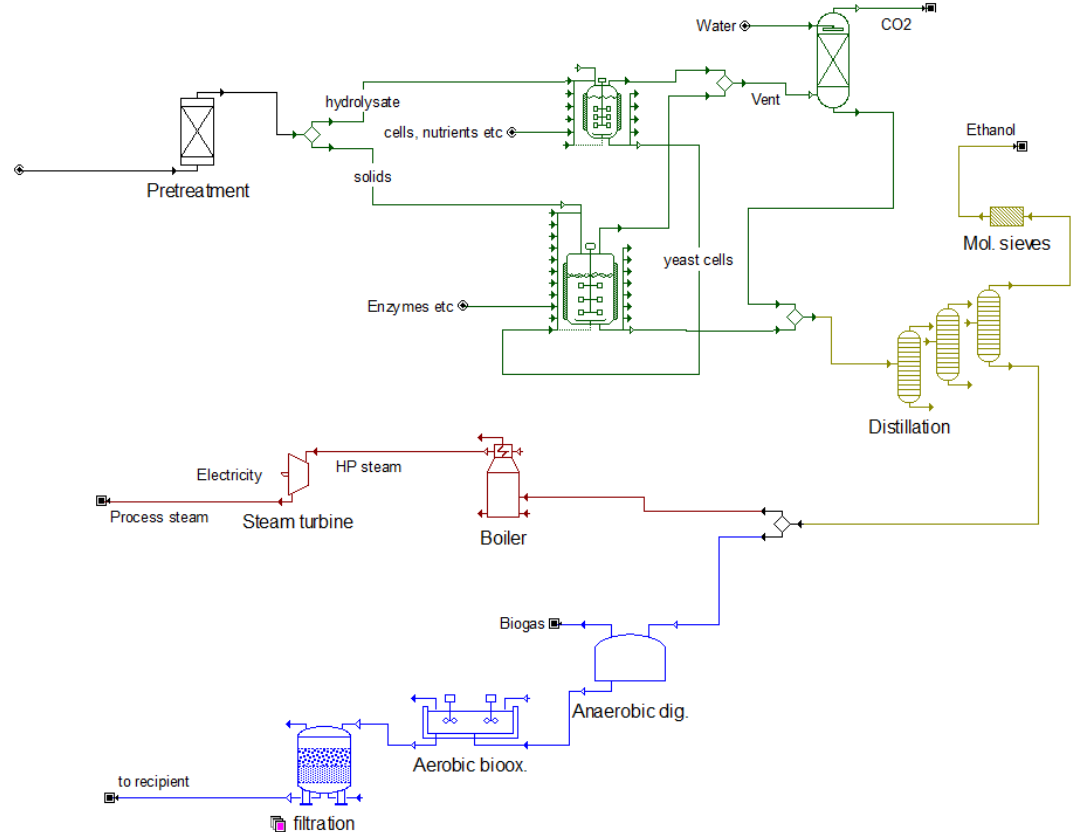
Experiments

Analyses

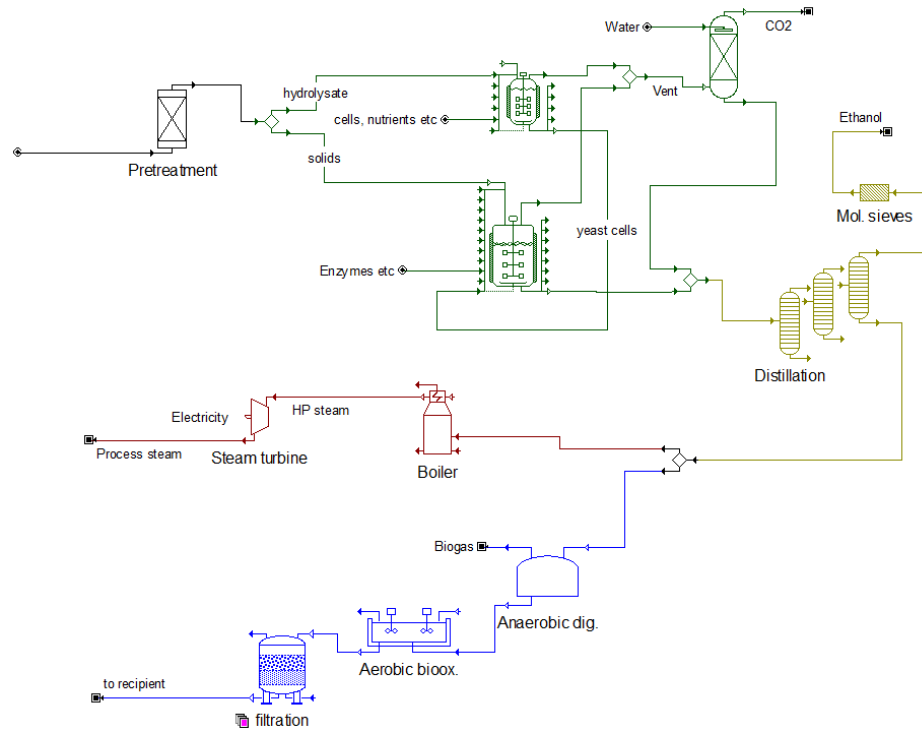
External
sources

- Process design
- Reactions
- Scheduling
- Utility systems
- Up/downstream units

Pinch
analysis



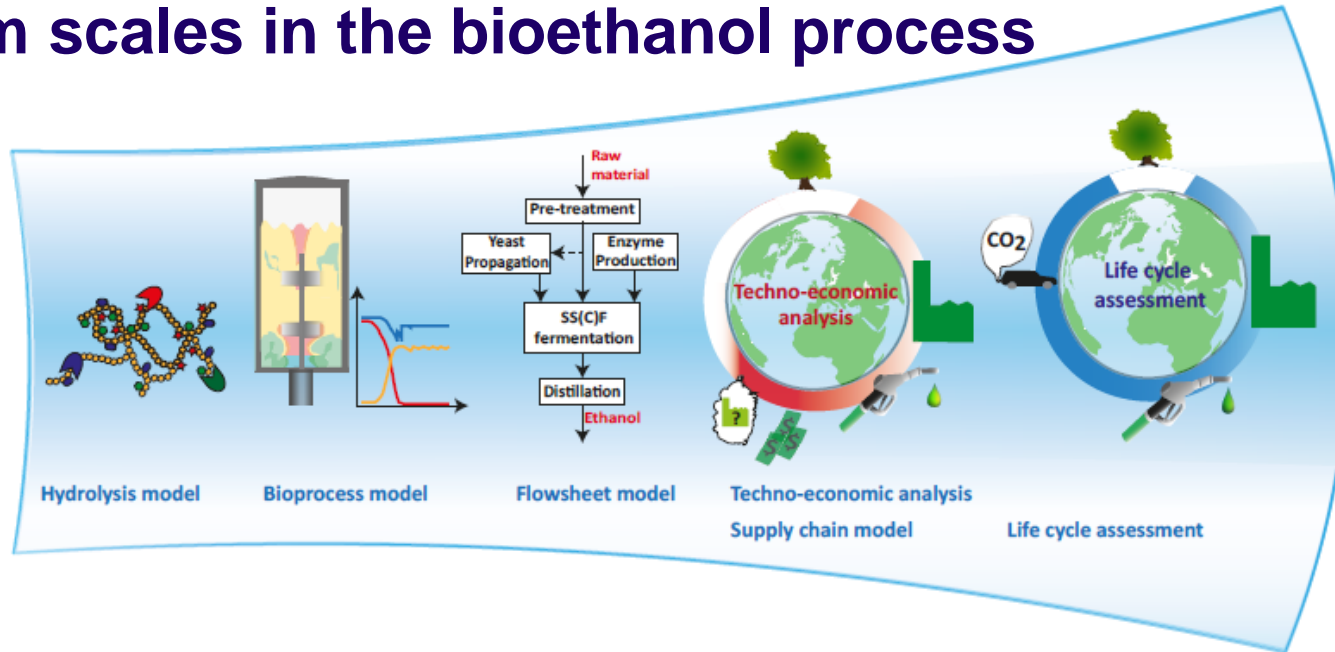
Flowsheet model– the outputs



mass/energy balances to:

- 🎯 **Techno-Economic Estimates**
- 🎯 **Supply chain analysis**
- 🎯 **Life cycle analysis**

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Life cycle assessment

- Calculates the potential environmental impact of ethanol production

- Inputs:

Database

Bioreactor model

Flowsheet model

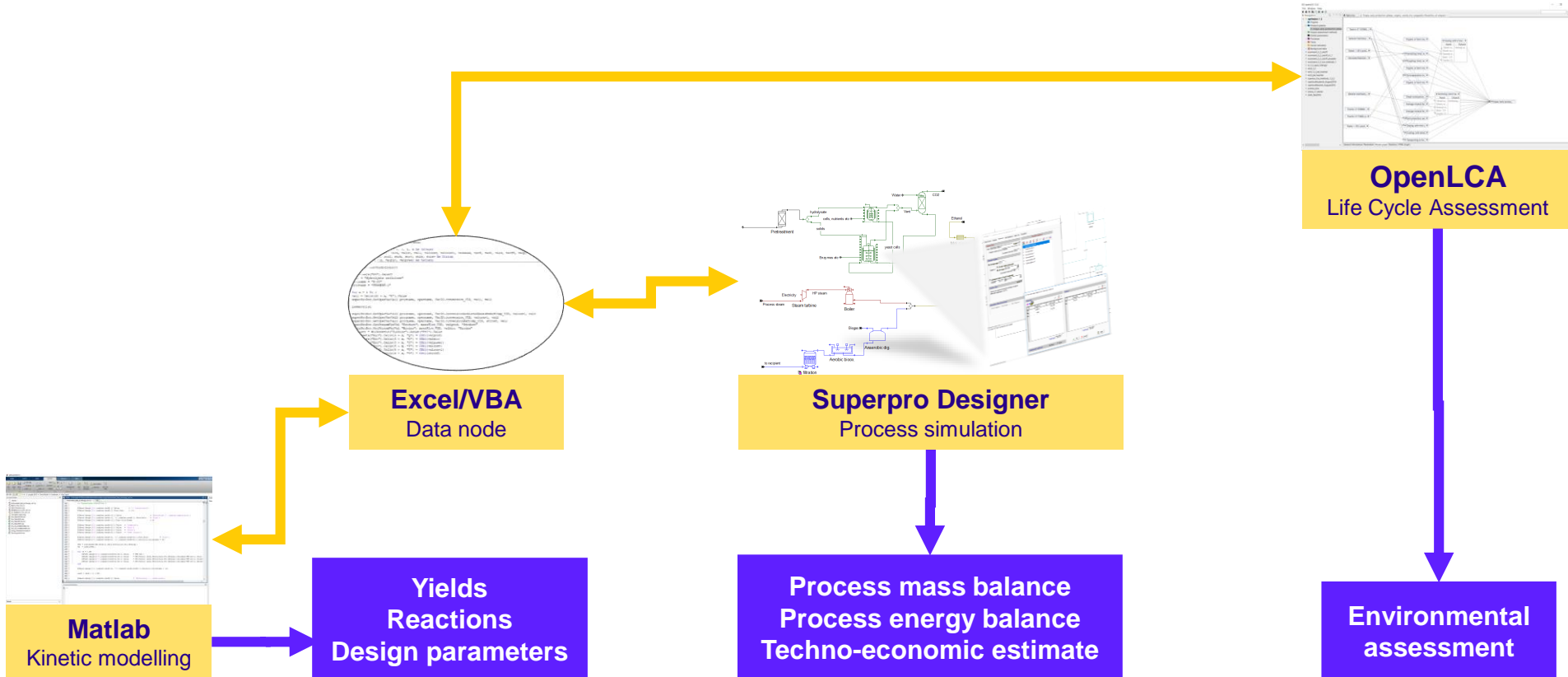
- Software: openLCA

Contribution tree: Cellic CTec2, PEG, 30% DM, 7.5 FPU, PSSF

Flow: Impact category:

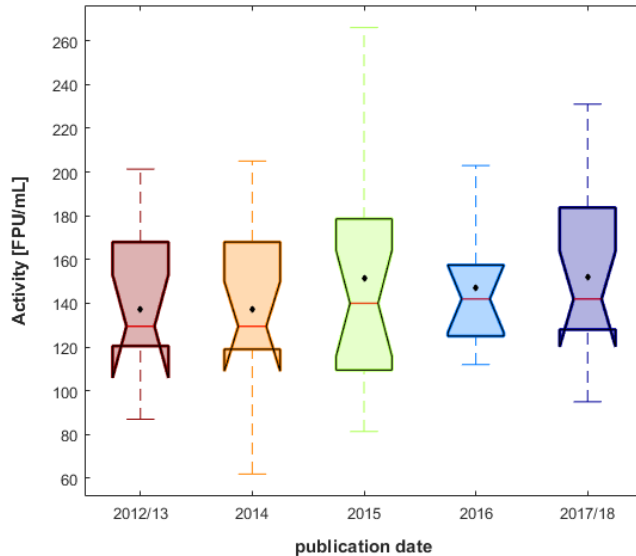
Contribution	Process	Amount	Unit
100.00%	ethanol, product, PEG, Cellic CTec2, 30% DM, 7.5 FPU, PSSF	2.56378	kg CO2-Eq
99.43%	ethanol, fermentation, PEG, Cellic CTec2, 30% DM, 7.5 FPU, PSSF	2.54920	kg CO2-Eq
75.59%	enzyme, Cellic CTec2 - DK	1.93798	kg CO2-Eq
20.26%	straw, pretreated - DK	0.51942	kg CO2-Eq
19.43%	straw, prepared - DK	0.49810	kg CO2-Eq
18.29%	wheat IP - CH	0.46904	kg CO2-Eq
00.74%	transport, lorry >16t, fleet average - RER	0.01902	kg CO2-Eq
00.39%	electricity mix - DK	0.01004	kg CO2-Eq
00.83%	Combustion, dry wood residue, AP-42 (burning lignin) - RNA	0.02132	kg CO2-Eq
02.02%	Polyethylene glycol	0.05182	kg CO2-Eq
00.86%	sodium hydroxide, 50% in H2O, production mix, at plant - RER	0.02205	kg CO2-Eq
00.70%	whey, to fermentation - CH	0.01792	kg CO2-Eq
00.57%	Combustion, dry wood residue, AP-42 (burning lignin) - RNA	0.01458	kg CO2-Eq

Data flow between scales

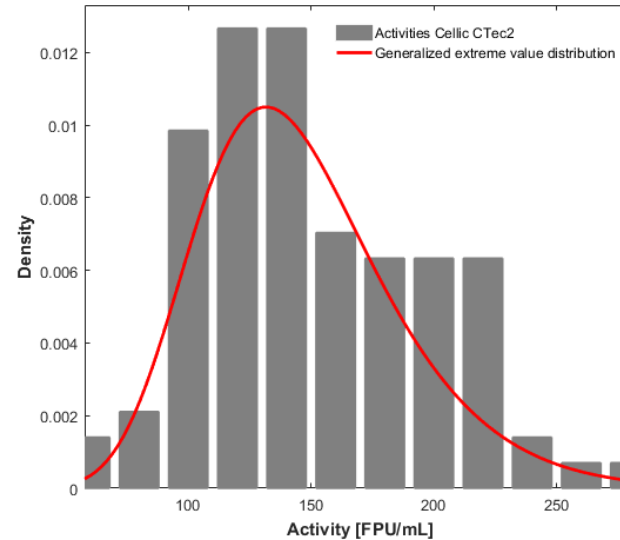


Variability in enzymatic activities – a case study

Step 1: Data collection



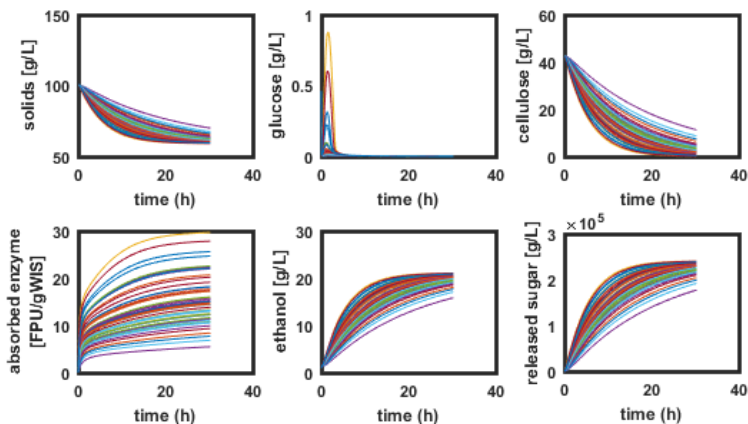
Step 2: Distribution fit



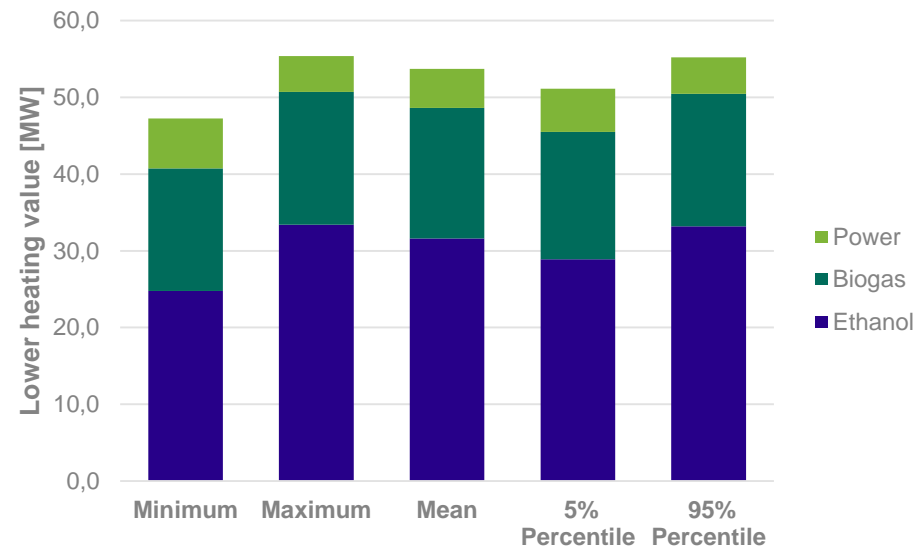
- Generalized extreme value distribution

Variability in enzymatic activities – a case study

Step 3: Propagation in bioprocess model



Step 4: Techno-economic assessment



The multi-scale concept:

- includes variability assessment in **early process development**
- allows to determine **stable process configurations**
- allows for **multi-objective optimization**
- shall allow to determine **optimal experimental conditions** to perform model validation experiments
- Ongoing: Include life cycle assessment in calculations



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